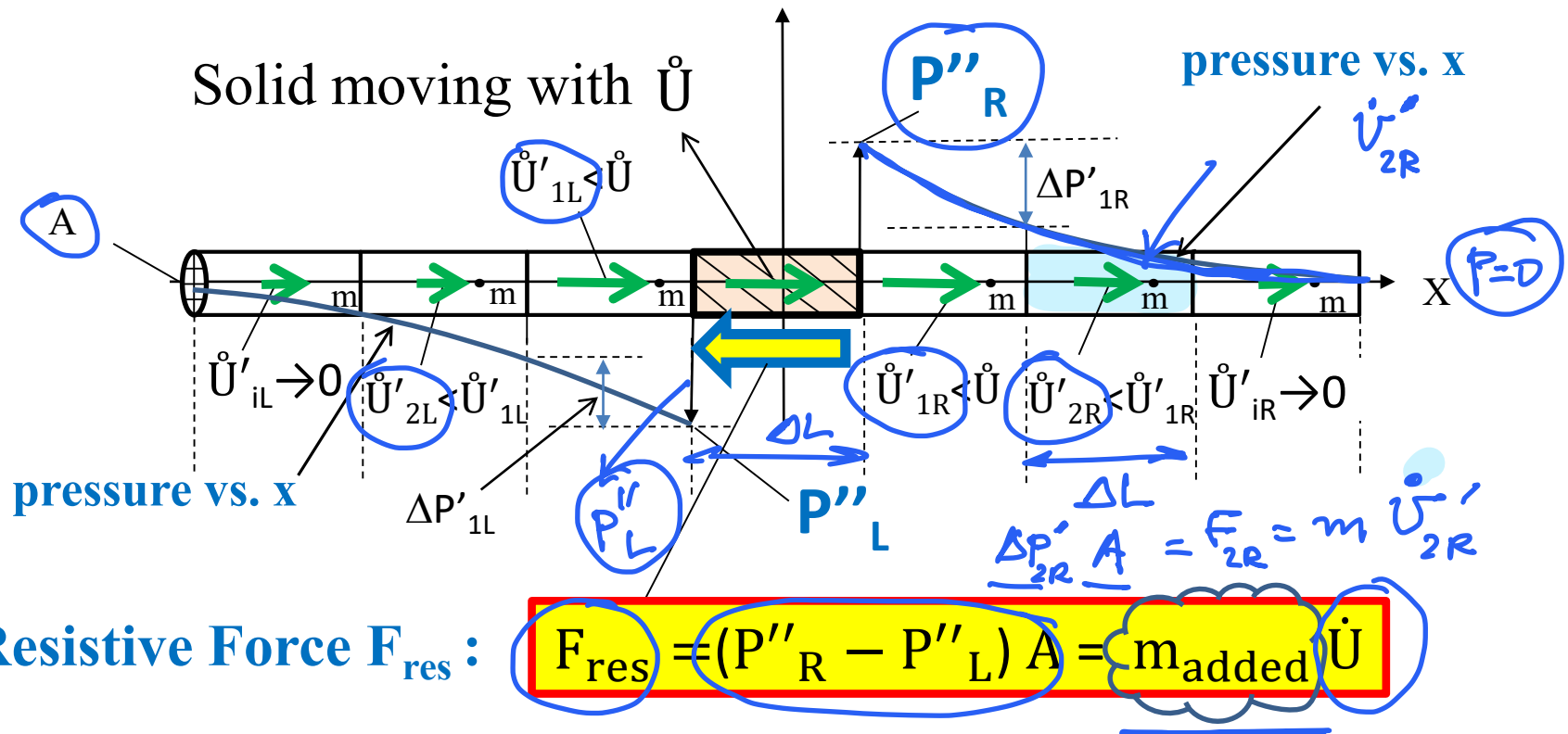


The concept of Added Mass (1/7)

Solid moving with acceleration $\ddot{U}$ inside quiescent fluid

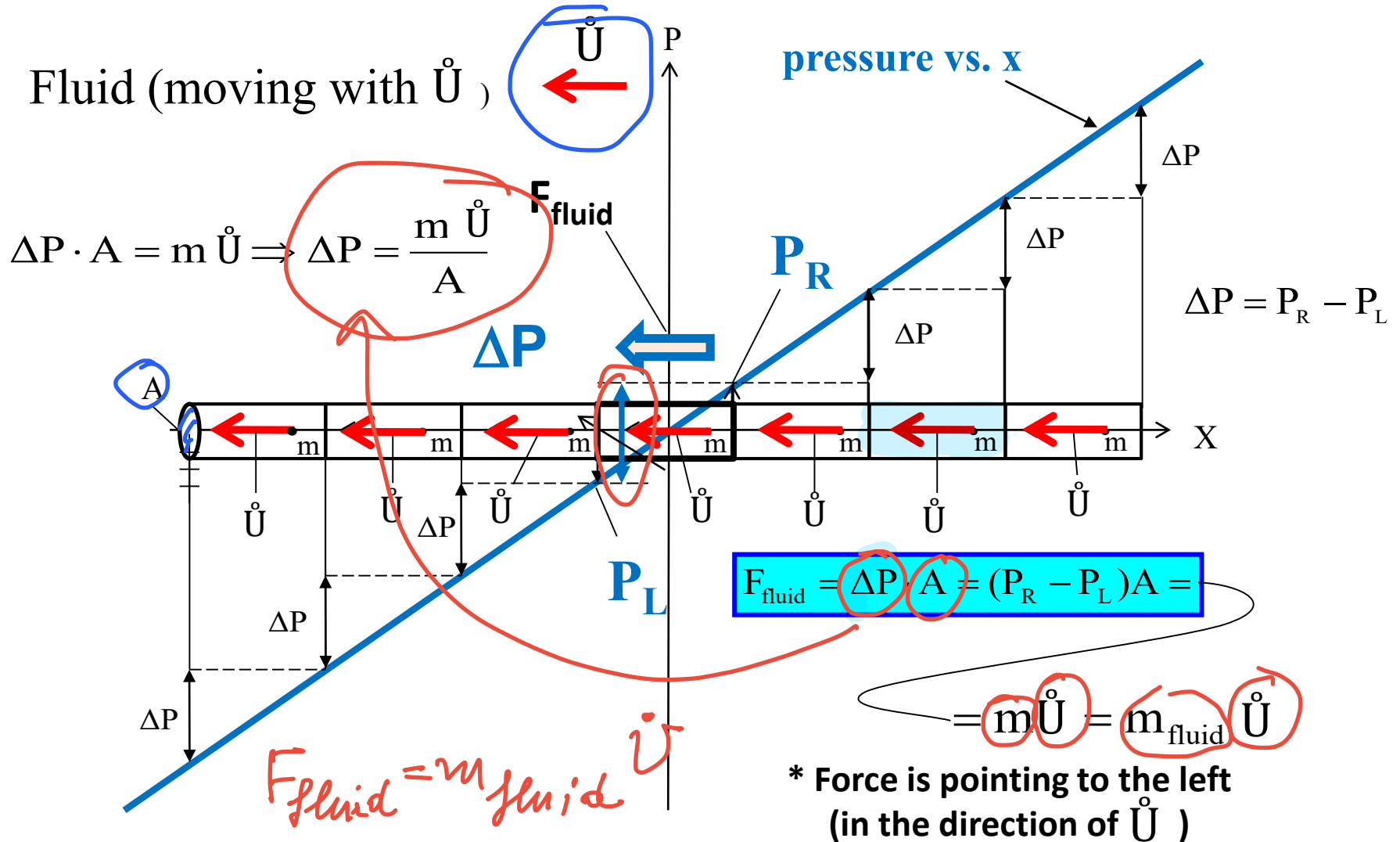


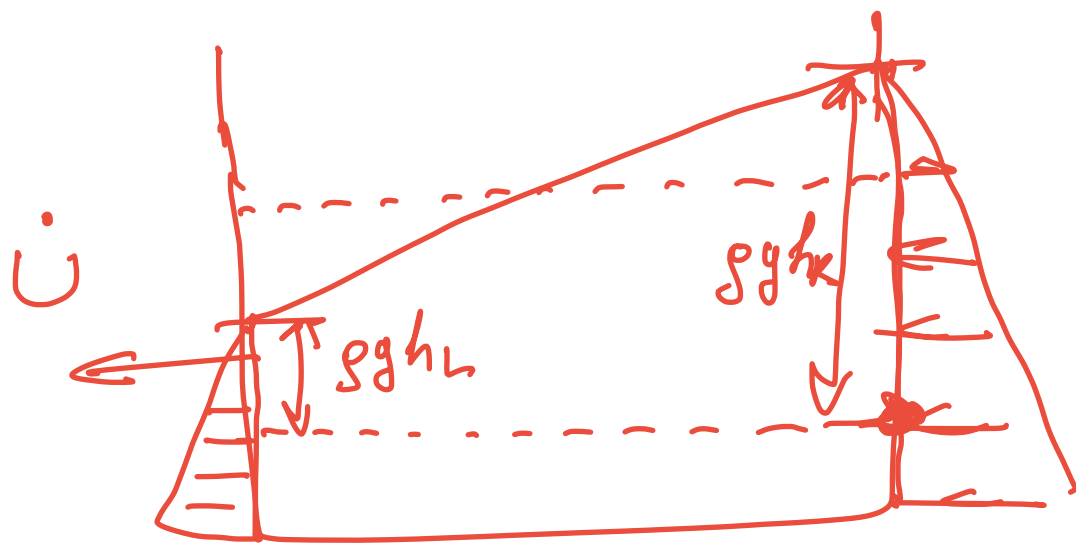
$$F_{res} = (P''_R - P''_L) A = \sum \Delta P'_{iR} A + \sum \Delta P'_{iL} A = \sum m \ddot{U}'_{iR} + \sum m \ddot{U}'_{iL}$$

The resistive force ($F_{res} = m_{added} \ddot{U}$) is needed in order to accelerate parts of the surrounding fluid which move with the body.

The concept of Added Mass (2/7)

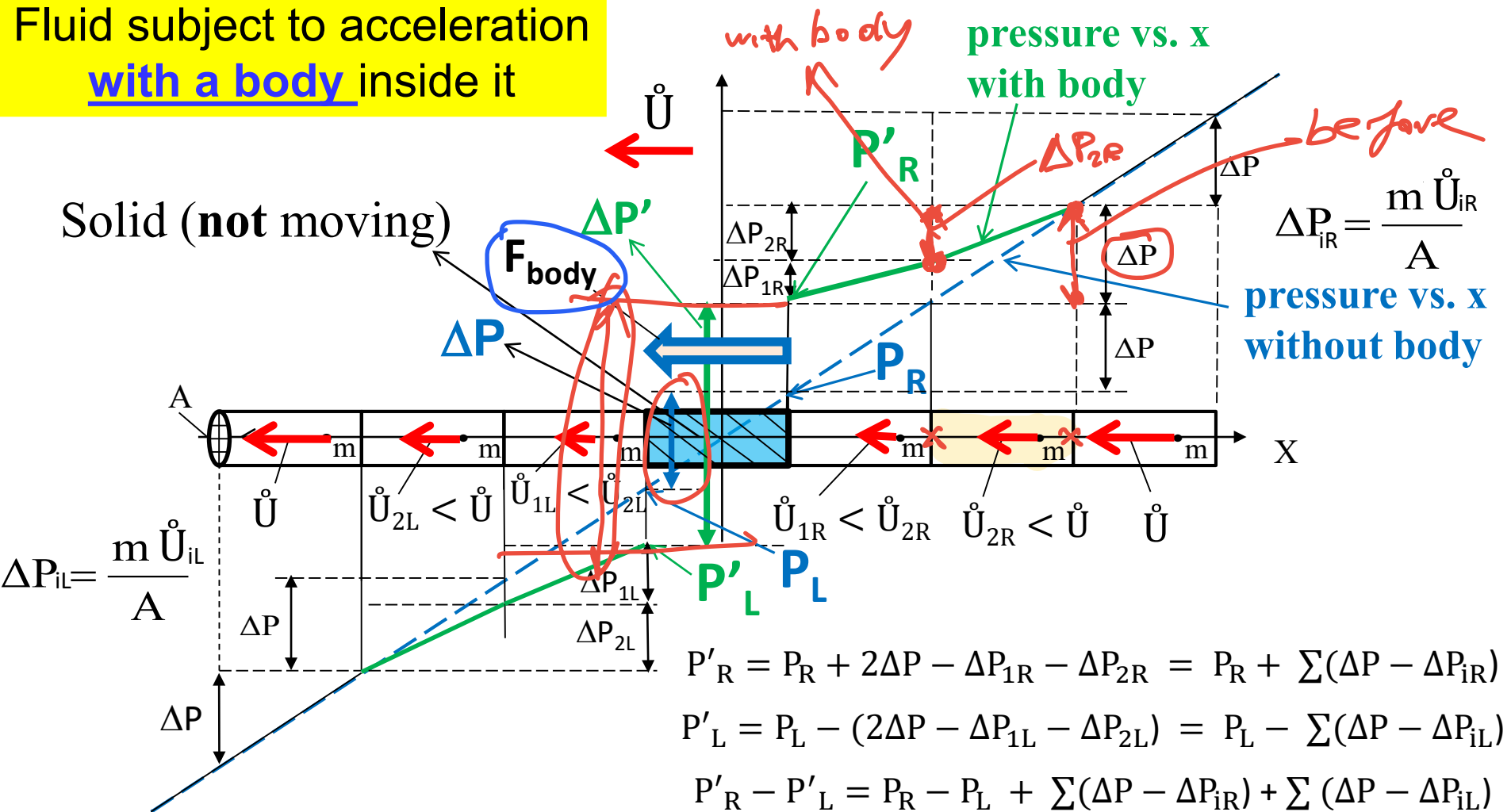
Fluid subject to acceleration without a body inside it





The concept of Added Mass (3/7)

Fluid subject to acceleration
with a body inside it



$$F_{\text{body}} = (P'_R - P'_L) A = (P_R - P_L) A + \sum m (\dot{U} - \dot{U}_{iR}) + \sum m (\dot{U} - \dot{U}_{iL})$$

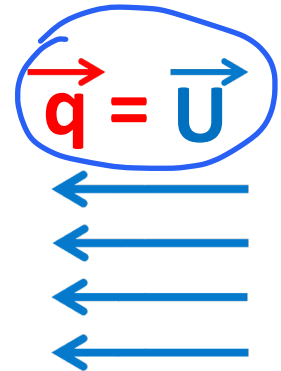
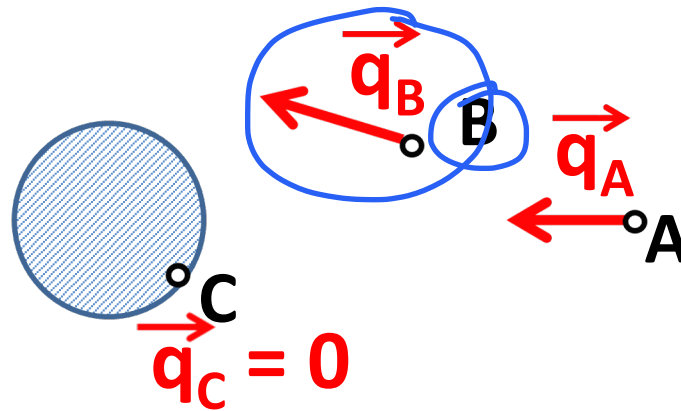
$$\underline{F_{\text{body}}} = \underline{m_{\text{fluid}}} \underline{\dot{U}} + \underline{\sum m (\dot{U} - \dot{U}_{iR})} + \underline{\sum m (\dot{U} - \dot{U}_{iL})}$$

← addition
you
force³

The concept of Added Mass (4/7)

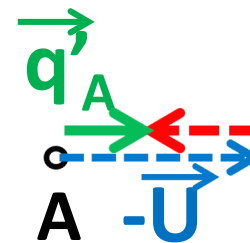
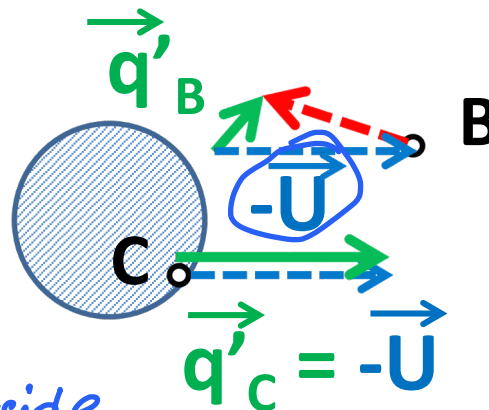
Two Different Frames of Reference (for the same problem!):

Body is stationary
and flow is moving
to the left with
speed U



$$\vec{q}' = \vec{q} - \vec{U}$$

Flow is stationary
(far upstream) and body
is moving to the right
with speed U



$$\vec{q}' = 0$$

The concept of Added Mass (5/7)

$$F_{\text{res}} = (P''_R - P''_L) A = \sum m \dot{U}'_{iR} + \sum m \dot{U}'_{iL} = m_{\text{added}} \dot{U}$$

$$\dot{U}'_{iR} = -\dot{U}_{iR} - (-\dot{U}) = \dot{U} - \dot{U}_{iR}$$

$$\dot{U}'_{iL} = -\dot{U}_{iL} - (-\dot{U}) = \dot{U} - \dot{U}_{iL}$$

Thus:

$$\sum m (\dot{U} - \dot{U}_{iR}) + \sum m (\dot{U} - \dot{U}_{iL}) = m_{\text{added}} \dot{U}$$

$$F_{\text{body}} = m_{\text{fluid}} \dot{U} + \sum m (\dot{U} - \dot{U}_{iR}) + \sum m (\dot{U} - \dot{U}_{iL})$$

Thus:

$$F_{\text{body}} = m_{\text{fluid}} \dot{U} + m_{\text{added}} \dot{U} = (m_{\text{fluid}} + m_{\text{added}}) \dot{U}$$

$$F_{\text{body}} = F_{\text{inertial}} = C_M m_{\text{fluid}} \ddot{U}$$

Inertia coefficient C_M

$$C_M = \frac{F_{\text{body}}}{F_{\text{fluid}}}$$

$$C_M = \frac{m_{\text{fluid}} + m_{\text{added}}}{m_{\text{fluid}}}$$

➤ m_{fluid} = mass of fluid displaced by body

➤ m_{added} = added mass; function of body shape and inflow direction

The concept of Added Mass (6/7)

Definition of inertia coefficient C_M

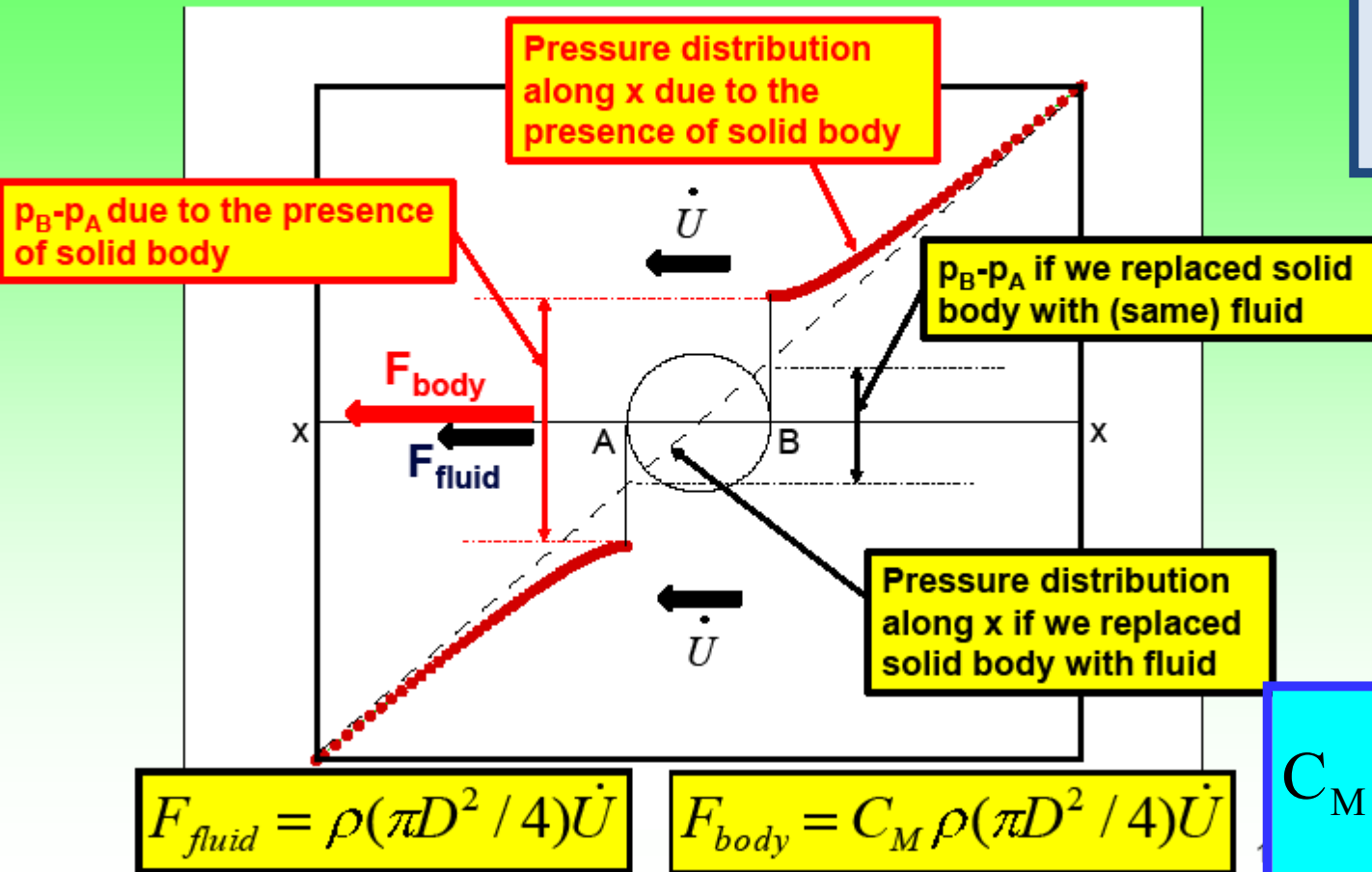
Cylinder subject to accelerated inflow.

Results from Inviscid flow simulation

$$C_M = \frac{F_{\text{body}}}{F_{\text{fluid}}}$$

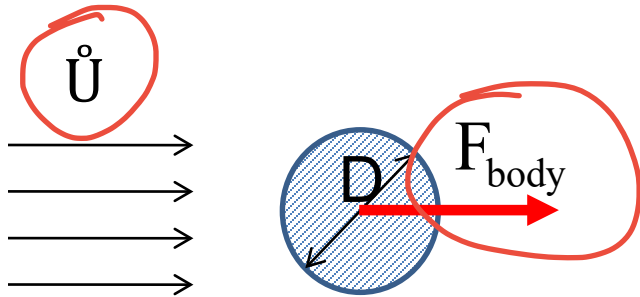
$$C_M = \frac{m_{\text{fluid}} + m_{\text{added}}}{m_{\text{fluid}}}$$

For inviscid flow around 2-D cylinder: $C_M=2$



The concept of Added Mass (7/7)

Summary:(all quantities are per unit width in 2-D)



$$F_{\text{body}} = C_M m_{\text{fluid}} \dot{U}$$

$m_{\text{fluid}} = \rho_{\text{fluid}} V_{\text{fluid}}$ = mass of displaced fluid
 V_{fluid} = volume of displaced fluid

$$C_M = \text{inertia coefficient} = \frac{m_{\text{fluid}} + m_{\text{added}}}{m_{\text{fluid}}} = 1 + \frac{m_{\text{added}}}{m_{\text{fluid}}} = 1 + a$$

$$a = \frac{m_{\text{added}}}{m_{\text{fluid}}} = \text{added mass coefficient (depends on shape + direction of flow)}$$

and inviscid flow

For a cylinder (circle in 2-D) V_{fluid} = area of cross section = $\pi D^2 / 4$

For a cylinder in inviscid unbounded flow: $C_M = 2$ ($a = 1$)

Handwritten note: $m_{\text{fluid}} = \rho V_{\text{fluid}} = \rho \frac{\pi D^2}{4}$

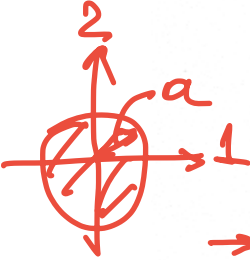
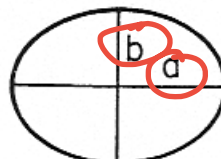
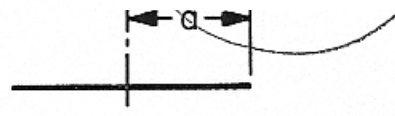
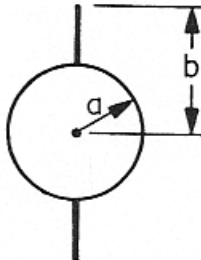
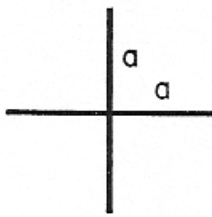
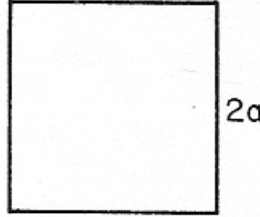
(Inviscid) Added Mass for other shapes:

m_{11} and m_{22} are the added masses when the flow is accelerated in the horizontal or the vertical axis, respectively. m_{66} is the added moment of inertia when the body rotates around an axis normal to the paper.

Table 4.3

Added-Mass Coefficients for Various Two-Dimensional Bodies.

Assumes inviscid flow

			
$\rightarrow m_{11}:$ $\pi \rho a^2$ $\rightarrow m_{22}:$ $\pi \rho a^2$ $m_{66}:$ 0	$\Rightarrow m_{11}:$ $\pi \rho a^2$ $\Rightarrow m_{22}:$ $\pi \rho a^2$ $m_{66}:$ 0	$\Rightarrow m_{11}:$ $\pi \rho b^2$ $\Rightarrow m_{22}:$ $\pi \rho a^2$ $m_{66}:$ $\frac{1}{8} \pi \rho (a^2 - b^2)^2$	$m_{11}:$ 0 $m_{22}:$ $\pi \rho a^2$ $m_{66}:$ $\frac{1}{8} \pi \rho a^4$
			
$m_{11}:$ $\pi \rho [a^2 + (b^2 - a^2)^2 / b^2]$ $m_{22}:$ $\pi \rho a^2$ $m_{66}:$ *	$m_{11}:$ $\pi \rho a^2$ $m_{22}:$ $\pi \rho a^2$ $m_{66}:$ $\frac{2}{3} \pi \rho a^4$	$m_{11}:$ $4.754 \rho a^2$ $m_{22}:$ $4.754 \rho a^2$ $m_{66}:$ $0.725 \rho a^4$	

From Marine Hydrodynamics,
Newman, J.N., 1977

*For the finned circle the added moment of inertia is given by the formula

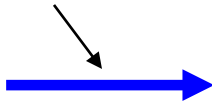
$$m_{66} = \rho a^4 (\pi^{-1} \csc^4 \alpha [2\alpha^2 - \alpha \sin 4\alpha + \frac{1}{2} \sin^2 2\alpha] - \pi/2)$$

~~*~~

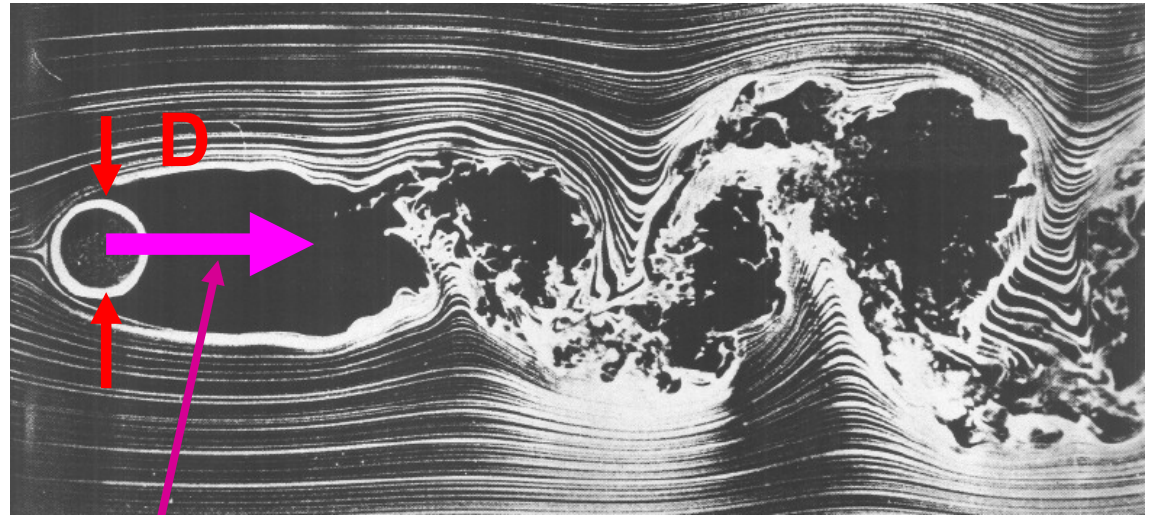
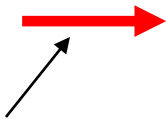
Morison's equation for total force in the direction of wave propagation

[Morison, J. R.; O'Brien, M. P.; Johnson, J. W.; Schaaf, S. A. (1950), "The force exerted by surface waves on piles", Petroleum Transactions (American Institute of Mining Engineers) 189: 149–154]

Velocity, u



Acceleration, a



Total force = Viscous force + Inertial force

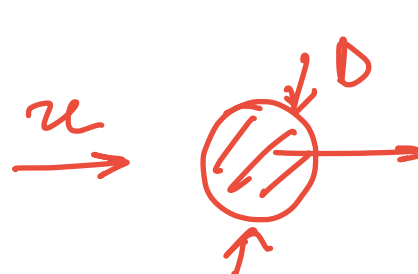
**Total force
(per unit width)**

$$C_D \frac{1}{2} \rho D u |u|$$

Drag coefficient

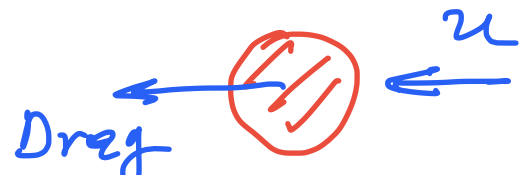
$$C_M \rho \frac{\pi D^2}{4} a$$

Inertia coefficient



$$\text{Drag} = C_D \frac{1}{2} \rho u^2 D$$

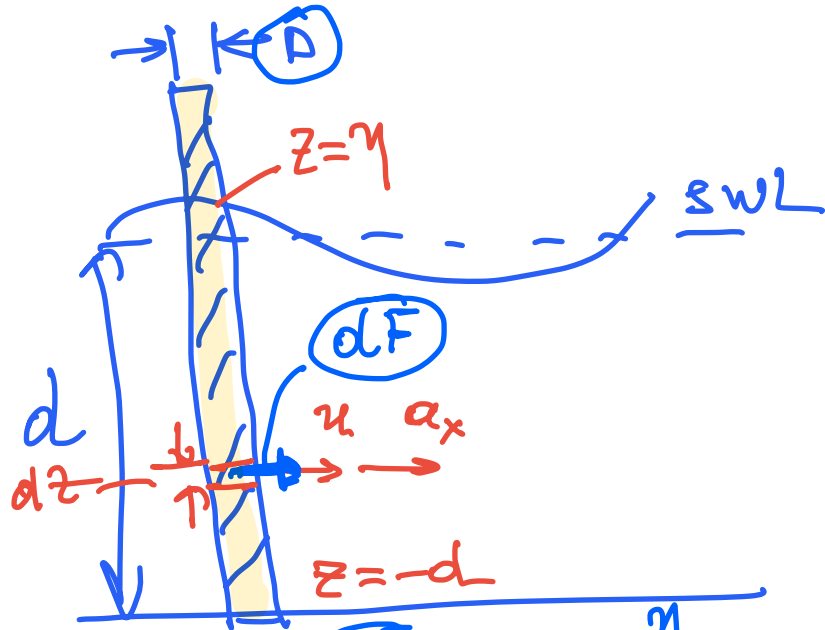
$$u > 0 \Rightarrow \text{Drag} > 0$$



$$C_D = C_D \frac{1}{2} \rho u^2 D$$

$$u < 0 \Rightarrow \text{Drag} < 0$$

$$\text{Drag} = C_D \frac{1}{2} \rho D |u|$$
 Using $|u|$ instead of u^2 guarantees that the Drag force is in the same direction as the inflow!



$$f_D = C_D \frac{\rho}{2} \underbrace{u|u|}_{\text{viscous force}} D$$

$$f_i = C_M \rho \frac{\pi D^2}{4} \underbrace{a_x}_{\text{inertial force}}$$

forces per unit depth

$$dF = f_D dz + f_i dz$$

$$F_t(t) = \int_{-d}^{\eta} dF = \int_{-d}^{\eta} f_D dz + \int_{-d}^{\eta} f_i dz = \underbrace{\int_{-d}^{\eta} f_D dz}_{\text{viscous force}} + \underbrace{\int_{-d}^{\eta} f_i dz}_{\text{inertial force}}$$

$$F_t(t) = F_D(t) + F_i(t)$$

$$F_i(t) = \int_{-d}^{\eta} C_M \rho \frac{\pi D^2}{4} a_x dz =$$

due to linear wave theory $\rightarrow 0$

$$= C_M \rho \frac{\pi D^2}{4} \int_{-d}^{\eta} a_x dz = C_M \rho \frac{\pi D^2}{4} \int_{-d}^{\eta} \frac{g\pi H}{L} \frac{\cosh[k(z+d)]}{\cosh[kd]} \sin \omega t dz$$

RELATIVE DEPTH	SHALLOW WATER $\frac{d}{L} < \frac{1}{25}$	TRANSITIONAL WATER $\frac{1}{25} < \frac{d}{L} < \frac{1}{2}$	DEEP WATER $\frac{d}{L} > \frac{1}{2}$
1. Wave profile	Same As $\rightarrow$	$\eta = \frac{H}{2} \cos \left[\frac{2\pi x}{L} - \frac{2\pi t}{T} \right] = \frac{H}{2} \cos \theta$	Same As $\leftarrow$
2. Wave celerity	$C = \frac{L}{T} = \sqrt{gd}$	$C = \frac{L}{T} = \frac{gT}{2\pi} \tanh \left(\frac{2\pi d}{L} \right)$	$C = C_0 = \frac{L}{T} = \frac{gT}{2\pi}$
3. Wavelength	$L = T \sqrt{gd} = CT$	$L = \frac{gT^2}{2\pi} \tanh \left(\frac{2\pi d}{L} \right)$	$L = L_0 = \frac{gT^2}{2\pi} = C_0 T$
4. Group velocity	$C_g = C = \sqrt{gd}$	$C_g = nC = \frac{1}{2} \left[1 + \frac{4\pi d/L}{\sinh(4\pi d/L)} \right] C$	$C_g = \frac{1}{2} C = \frac{gT}{4\pi}$
5. Water Particle Velocity			
(a) Horizontal	$u = \frac{H}{2} \sqrt{\frac{g}{d}} \cos \theta$	$u = \frac{H}{2} \frac{gT}{L} \frac{\cosh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} \cos \theta$	$u = \frac{\pi H}{T} e^{\frac{2\pi z}{L}} \cos \theta$
(b) Vertical	$w = \frac{H\pi}{T} \left(1 + \frac{z}{d}\right) \sin \theta$	$w = \frac{H}{2} \frac{gT}{L} \frac{\sinh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} \sin \theta$	$w = \frac{\pi H}{T} e^{\frac{2\pi z}{L}} \sin \theta$
6. Water Particle Accelerations			
(a) Horizontal	$a_x = \frac{H\pi}{T} \sqrt{\frac{g}{d}} \sin \theta$	$a_x = \frac{g\pi H}{L} \frac{\cosh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} \sin \theta$	$a_x = 2H \left(\frac{\pi}{T}\right)^2 e^{\frac{2\pi z}{L}} \sin \theta$
(b) Vertical	$a_z = -2H \left(\frac{\pi}{T}\right)^2 \left(1 + \frac{z}{d}\right) \cos \theta$	$a_z = -\frac{g\pi H}{L} \frac{\sinh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} \cos \theta$	$a_z = -2H \left(\frac{\pi}{T}\right)^2 e^{\frac{2\pi z}{L}} \cos \theta$
7. Water Particle Displacements			
(a) Horizontal	$\xi = -\frac{HT}{4\pi} \sqrt{\frac{g}{d}} \sin \theta$	$\xi = -\frac{H}{2} \frac{\cosh[2\pi(z+d)/L]}{\sinh(2\pi d/L)} \sin \theta$	$\xi = -\frac{H}{2} e^{\frac{2\pi z}{L}} \sin \theta$
(b) Vertical	$\zeta = \frac{H}{2} \left(1 + \frac{z}{d}\right) \cos \theta$	$\zeta = \frac{H}{2} \frac{\sinh[2\pi(z+d)/L]}{\sinh(2\pi d/L)} \cos \theta$	$\zeta = \frac{H}{2} e^{\frac{2\pi z}{L}} \cos \theta$
8. Subsurface Pressure	$p = \rho g (\eta - z)$	$p = \rho g \eta \frac{\cosh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} - \rho g z$	$p = \rho g \eta e^{\frac{2\pi z}{L}} - \rho g z$

Figure 2-6. Summary of linear (Airy) wave theory--wave characteristics.

$$\rightarrow = C_M \rho \frac{\pi D^2}{4} H g \int_{-d}^0 \frac{\pi}{L} \frac{\cosh[k(z+d)]}{\cosh[kd]} dz \sin \theta$$

$$K_{im} = \frac{1}{2} \tanh\left(\frac{2\pi d}{L}\right)$$

$$\Rightarrow \underline{F_i(t) = F_{im} \sin \theta}$$

$$\underline{\theta = kx - \omega t}$$

$$F_{im} = C_M \rho \frac{\pi D^2}{4} H \cdot K_{im}$$

↪ maximum inertial force

Similarly it can be derived that:

$$F_D(t) = \int_{-d}^0 f_D dz = F_{Dm} |\cos \theta| \cos \theta$$

$$F_{Dm} = C_D \frac{1}{2} \rho g D H^2 K_{Dm}$$

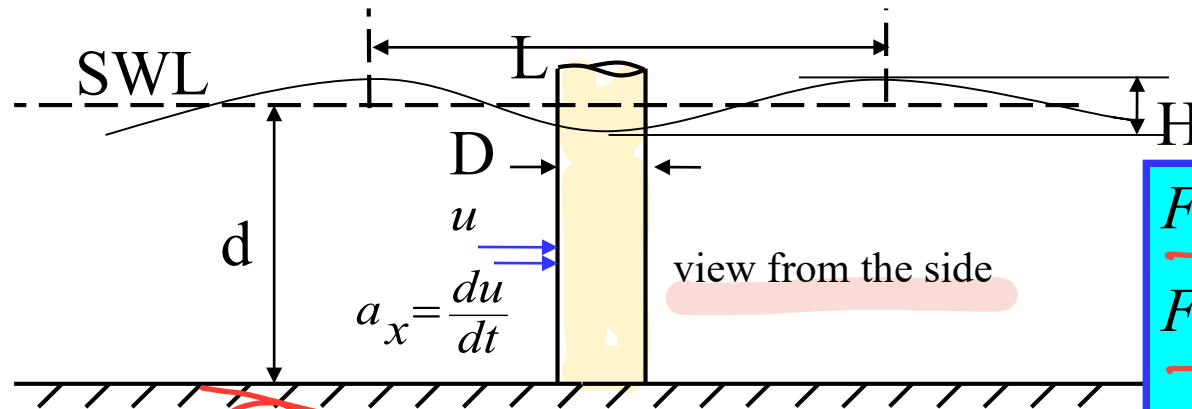
↪ maximum drag force

$$K_{Dm} = \frac{1}{8} \left[1 + \frac{\frac{4\pi d}{L}}{\sinh\left[\frac{4\pi d}{L}\right]} \right]$$

$$\rightarrow = \frac{\eta}{4} \quad \eta: C_D/C_M$$

Application of Morison's equation to determine forces on vertical piles

Morison's equation is integrated over the length of the pile, after the values for u and a_x have been determined by either using linear or non-linear wave theories



$$\vartheta = -\omega t$$

$$F_{total}(t) = F_i(t) + F_D(t)$$

$$F_i(t) = F_{im} \cdot \sin(\vartheta)$$

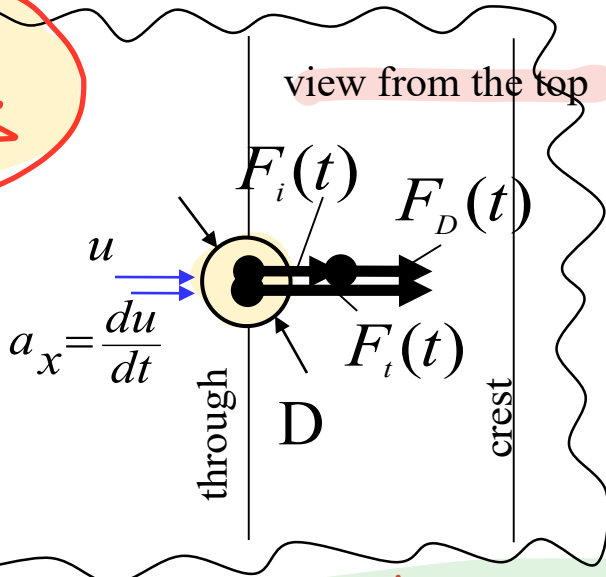
$$F_{im} = C_M \cdot \rho g \cdot \frac{\pi D^2}{4} H \cdot K_{im}$$

$$F_D(t) = F_{Dm} \cdot |\cos \vartheta| \cos \vartheta$$

$$F_{Dm} = C_D \frac{1}{2} \rho g D H^2 \cdot K_{Dm}$$

APPLY ONLY FOR FULL PILES

extending from seabed to free surface



For deep H₂O: $K_{im} = \frac{1}{2}$; $K_{Dm} = \frac{1}{8}$

$$K_{im} = \frac{1}{2} \tanh\left(\frac{2\pi d}{L}\right)$$

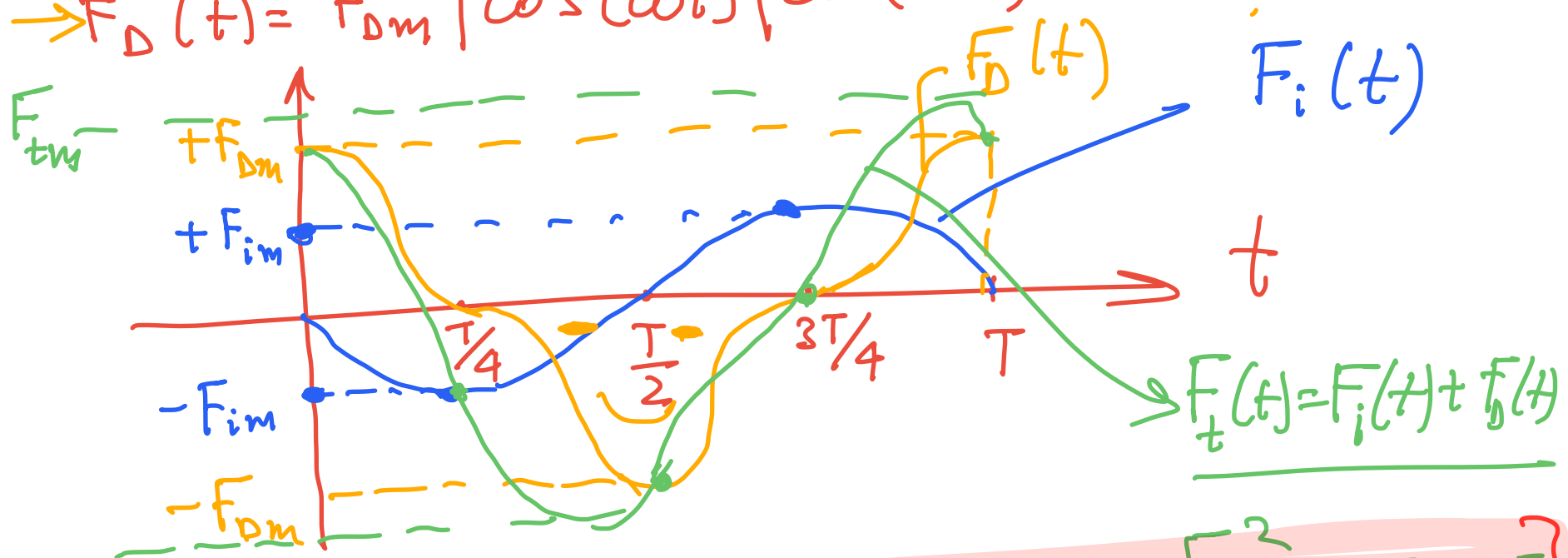
$$K_{DM} = \frac{1}{8} \left(1 + \frac{4\pi d / L}{\sinh[4\pi d / L]} \right) = \frac{\eta}{4}$$

$$\eta = c_g / c$$

$$x=0, \quad \vartheta = kx - \omega t = -\omega t$$

$$\rightarrow F_i(t) = F_{im} \sin(-\omega t) = -F_{im} \frac{\sin(\omega t)}{1}$$

$$\rightarrow F_D(t) = F_{Dm} |\cos(\omega t)| \overline{\cos(\omega t)}$$



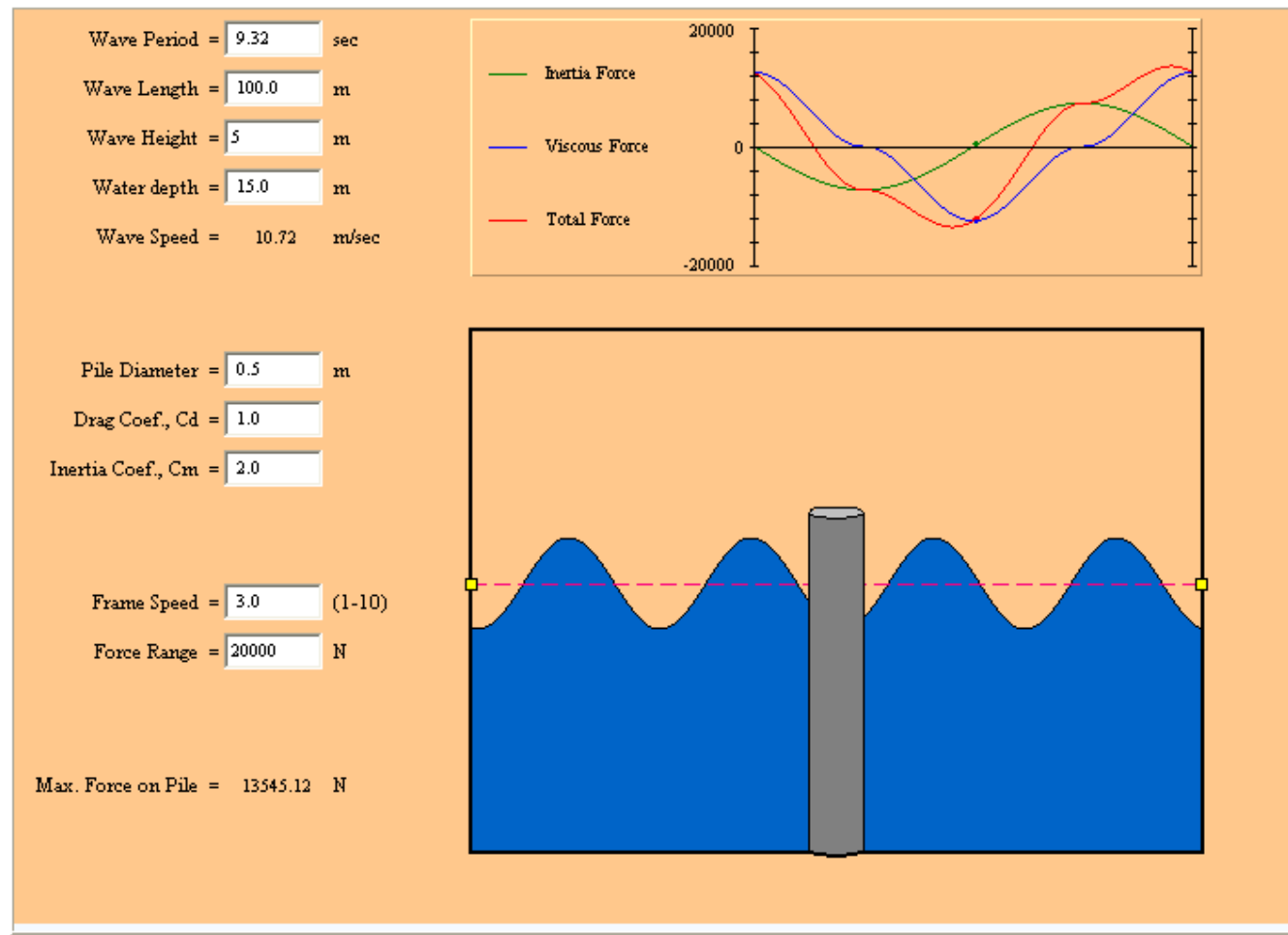
$\Rightarrow F_t(t) = F_i(t) + F_d(t)$

$-F_{tm}$

- $F_{tm} = \max$ total force $= F_{Dm} + \frac{F_{im}^2}{4F_{Dm}}$ if $\underline{F_{im}} < \underline{2F_{Dm}}$
- " " " " $= \underline{F_{im}}$ if $\underline{F_{im}} > \underline{2F_{Dm}}$

The wave forces applet sums-up the forces per pile slice over the pile length

http://cavity.ce.utexas.edu/kinnas/wow/public_html/waveroom/Applet/WaveForces/WaveForces.html



Typical values of the drag and inertia coefficients
From API's (American Petroleum Institute)
Recommended Practice 2A-WSD (Dec. 2000)

- $C_D = 0.65$ and $C_M = 1.6$
for smooth piles
- $C_D = 1.05$ and $C_M = 1.2$
for rough piles (due to
marine growth)

→ $C_p \uparrow$ since rougher surface

Note: The diameter of the pile, D , also increases with marine growth

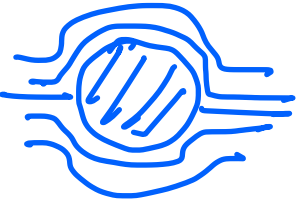


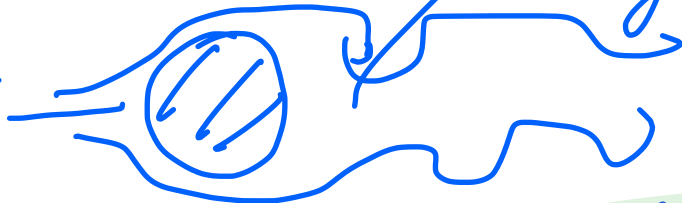
Yuck!

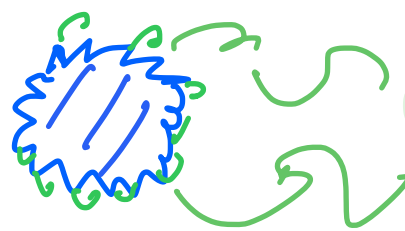
Q: Why C_M for smooth piles is less than 2,
and why is becoming ^{even} smaller for rough
piles?

$$C_M = 1 + a$$

$$a = \frac{m_{\text{added}}}{m_{\text{fluid}}} = \text{added mass coeff.}$$

inviscid  (no separation) ($a=1$ for cylinder in inviscid flow) $\Rightarrow C_M = 2$

viscous  $m_{\text{added}} \downarrow \Rightarrow a \downarrow \Rightarrow C_M \downarrow$
 $C_M < 2$ (body "accelerates" less fluid mass due to separated flow)

Rough Viscous  $C_M' < C_M$ $m_{\text{added}} \downarrow \downarrow \Rightarrow a \downarrow \downarrow \Rightarrow C_M \downarrow \downarrow$
 (body "accelerates" even less fluid mass due to additional separated flow at rough edges)

Total Force on Pile *(in the direction of wave propagation)*

Total force = Viscous force + Inertial force

Morison's equation

$$\sim C_D \rho D H^2 + \sim C_M \rho D^2 H$$

Drag coefficient

Inertia coefficient

Drag Force

Viscous force

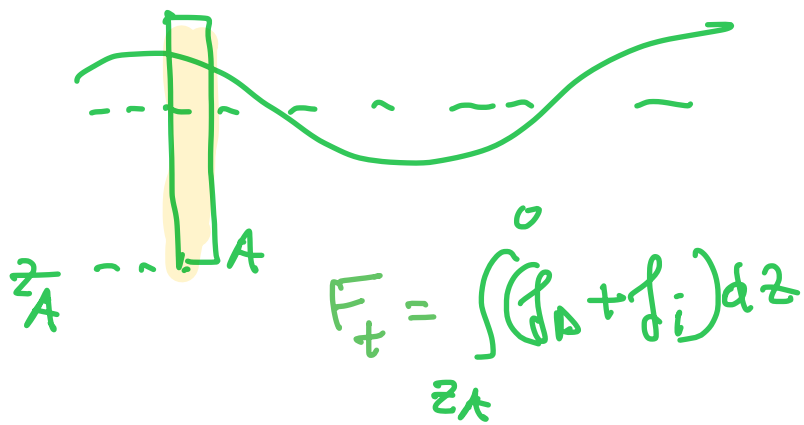
Inertial force

$\sim$

$$\frac{C_D}{C_M} \frac{H}{D}$$

As $H \uparrow$ or $D \downarrow$ or $H/D \uparrow$ the viscous forces become more important

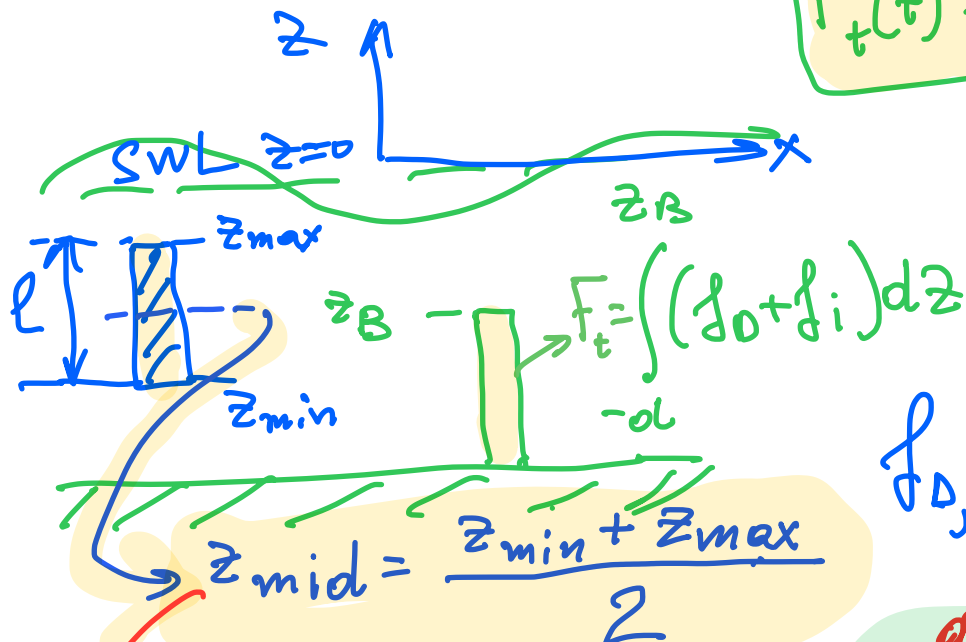
Short pile theory



$$F_i(t) = \int f_i dz \approx f_{i, \text{mid}} \ell$$

$$F_D(t) = \int_{z_{\min}}^{z_{\max}} f_D dz$$

$$F_t(t) = F_i(t) + F_D(t)$$



$$f_{i, \text{mid}} = C_M \rho \frac{\pi D^2}{4} a_{x, \text{mid}}$$

$$f_{D, \text{mid}} = C_D \frac{1}{2} \rho u_{\text{mid}} |u_{\text{mid}}| D$$

$a_{x, \text{mid}}$ and u_{mid} are values at the midpoint of the piles.

$$F_i(t) = F_{im} \sin \theta$$

$$F_D(t) = F_{Dm} |\cos \theta| \cos \theta$$

$$\underline{F_{im}} = f_{i, \text{mid}} \cdot l = C_M \rho \frac{\pi D^2}{4} a_{x, \text{mid}} \cdot l$$

$$\underline{F_{Dm}} = f_{D, \text{mid}} \cdot l = C_D \frac{1}{2} \rho u_{\text{mid}} |u_{\text{mid}}| \cdot D \cdot l$$

The formulas for F_{tm} , maximum
total force, still apply!

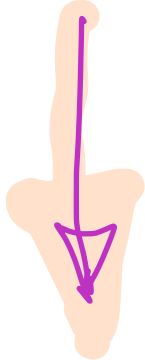
The values for $\underline{a_{x, \text{mid}}}$ and $\underline{u_{\text{mid}}}$
 can be found in Fig. 2-6



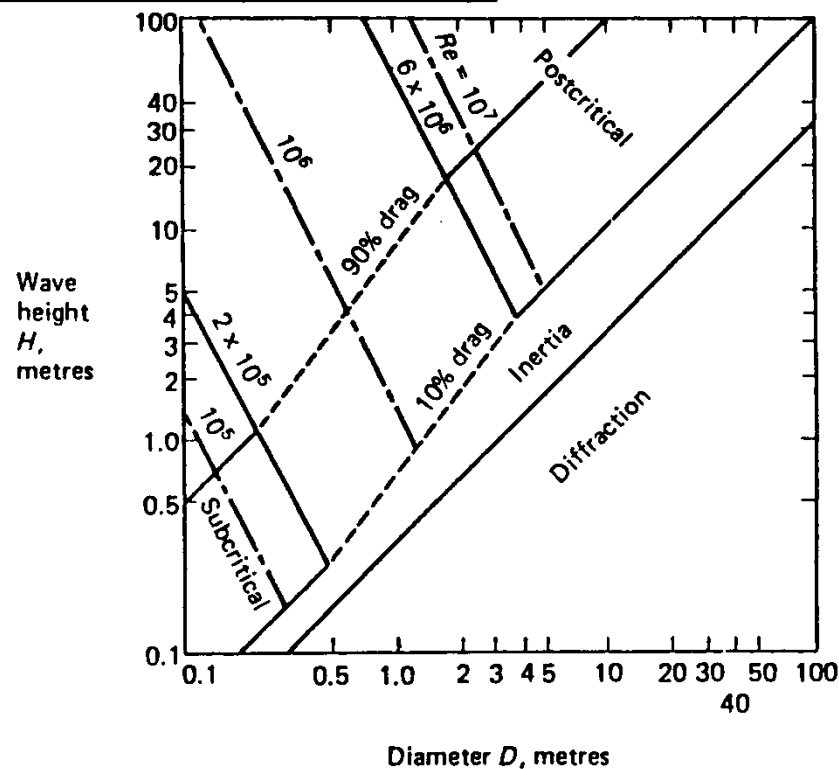
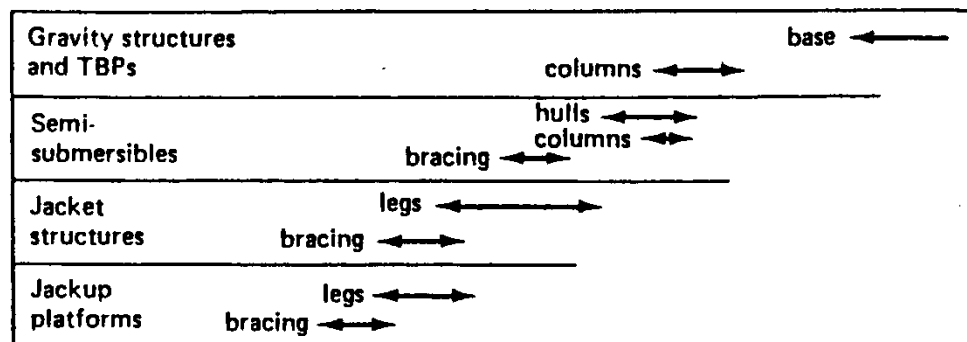
RELATIVE DEPTH	SHALLOW WATER $\frac{d}{L} < \frac{1}{25}$	TRANSITIONAL WATER $\frac{1}{25} < \frac{d}{L} < \frac{1}{2}$	DEEP WATER $\frac{d}{L} > \frac{1}{2}$
1. Wave profile	Same As $\rightarrow$	$\eta = \frac{H}{2} \cos \left[\frac{2\pi x}{L} - \frac{2\pi t}{T} \right] = \frac{H}{2} \cos \theta$	Same As $\leftarrow$
2. Wave celerity	$C = \frac{L}{T} = \sqrt{gd}$	$C = \frac{L}{T} = \frac{gT}{2\pi} \tanh \left(\frac{2\pi d}{L} \right)$	$C = C_0 = \frac{L}{T} = \frac{gT}{2\pi}$
3. Wavelength	$L = T \sqrt{gd} = CT$	$L = \frac{gT^2}{2\pi} \tanh \left(\frac{2\pi d}{L} \right)$	$L = L_0 = \frac{gT^2}{2\pi} = C_0 T$
4. Group velocity	$C_g = C = \sqrt{gd}$	$C_g = nC = \frac{1}{2} \left[1 + \frac{4\pi d/L}{\sinh(4\pi d/L)} \right] \cdot C$	$C_g = \frac{1}{2} C = \frac{gT}{4\pi}$
5. Water Particle Velocity			
(a) Horizontal	$u = \frac{H}{2} \sqrt{\frac{g}{d}} \cos \theta$	$u = \frac{H}{2} \frac{gT}{L} \frac{\cosh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} \cos \theta$	$u = \frac{\pi H}{T} e^{\frac{2\pi z}{L}} \cos \theta$
(b) Vertical	$w = \frac{H\pi}{T} \left(1 + \frac{z}{d}\right) \sin \theta$	$w = \frac{H}{2} \frac{gT}{L} \frac{\sinh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} \sin \theta$	$w = \frac{\pi H}{T} e^{\frac{2\pi z}{L}} \sin \theta$
6. Water Particle Accelerations			
(a) Horizontal	$a_x = \frac{H\pi}{T} \sqrt{\frac{g}{d}} \sin \theta$	$a_x = \frac{g\pi H}{L} \frac{\cosh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} \sin \theta$	$a_x = 2H \left(\frac{\pi}{T}\right)^2 e^{\frac{2\pi z}{L}} \sin \theta$
(b) Vertical	$a_z = -2H \left(\frac{\pi}{T}\right)^2 \left(1 + \frac{z}{d}\right) \cos \theta$	$a_z = -\frac{g\pi H}{L} \frac{\sinh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} \cos \theta$	$a_z = -2H \left(\frac{\pi}{T}\right)^2 e^{\frac{2\pi z}{L}} \cos \theta$
7. Water Particle Displacements			
(a) Horizontal	$\xi = -\frac{HT}{4\pi} \sqrt{\frac{g}{d}} \sin \theta$	$\xi = -\frac{H}{2} \frac{\cosh[2\pi(z+d)/L]}{\sinh(2\pi d/L)} \sin \theta$	$\xi = -\frac{H}{2} e^{\frac{2\pi z}{L}} \sin \theta$
(b) Vertical	$\zeta = \frac{H}{2} \left(1 + \frac{z}{d}\right) \cos \theta$	$\zeta = \frac{H}{2} \frac{\sinh[2\pi(z+d)/L]}{\sinh(2\pi d/L)} \cos \theta$	$\zeta = \frac{H}{2} e^{\frac{2\pi z}{L}} \cos \theta$
8. Subsurface Pressure	$p = \rho g (\eta - z)$	$p = \rho g \eta \frac{\cosh[2\pi(z+d)/L]}{\cosh(2\pi d/L)} - \rho g z$	$p = \rho g \eta e^{\frac{2\pi z}{L}} - \rho g z$

Figure 2-6. Summary of linear (Airy) wave theory--wave characteristics.

MATERIAL BELOW THIS LINE WAS NOT COVERED AND WILL NOT BE INCLUDED IN TEST II!



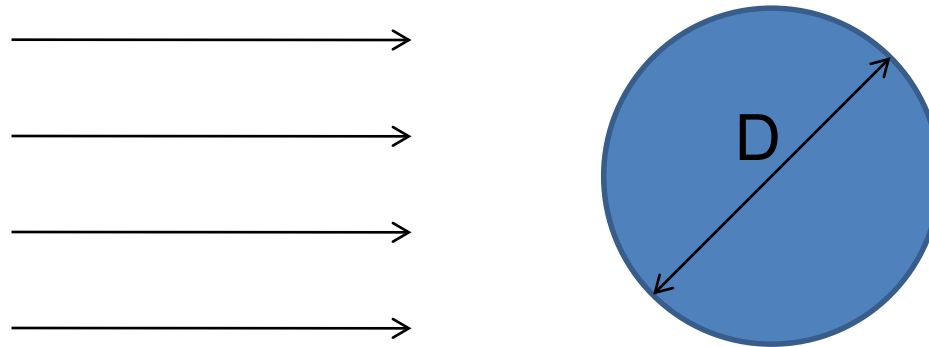
Effect of wave height H and diameter of element D on importance of viscous forces



An assessment of Morison's equation using CFD (Computational Fluid Dynamics)

Two Dimensional Cylinder in Oscillatory Flow

$$U = U_m \cdot \cos(\omega t)$$



Two important numbers:

- **Re (Reynolds No) = $U_m D / \nu$**
- **KC (Keulegan-Carpenter No) = $U_m T / D$ ($T = 2\pi / \omega$)**
~(distance the particles travel in T)/D

Morison's Equation

The inline force (force in the direction of the flow) is the sum of the drag force and the inertia force (per unit width)

$$F = \frac{1}{2} \rho C_D D |U| U + \frac{1}{4} \rho \pi D^2 C_M \frac{dU}{dt}$$

$$U = U_m \cdot \cos(\omega t)$$

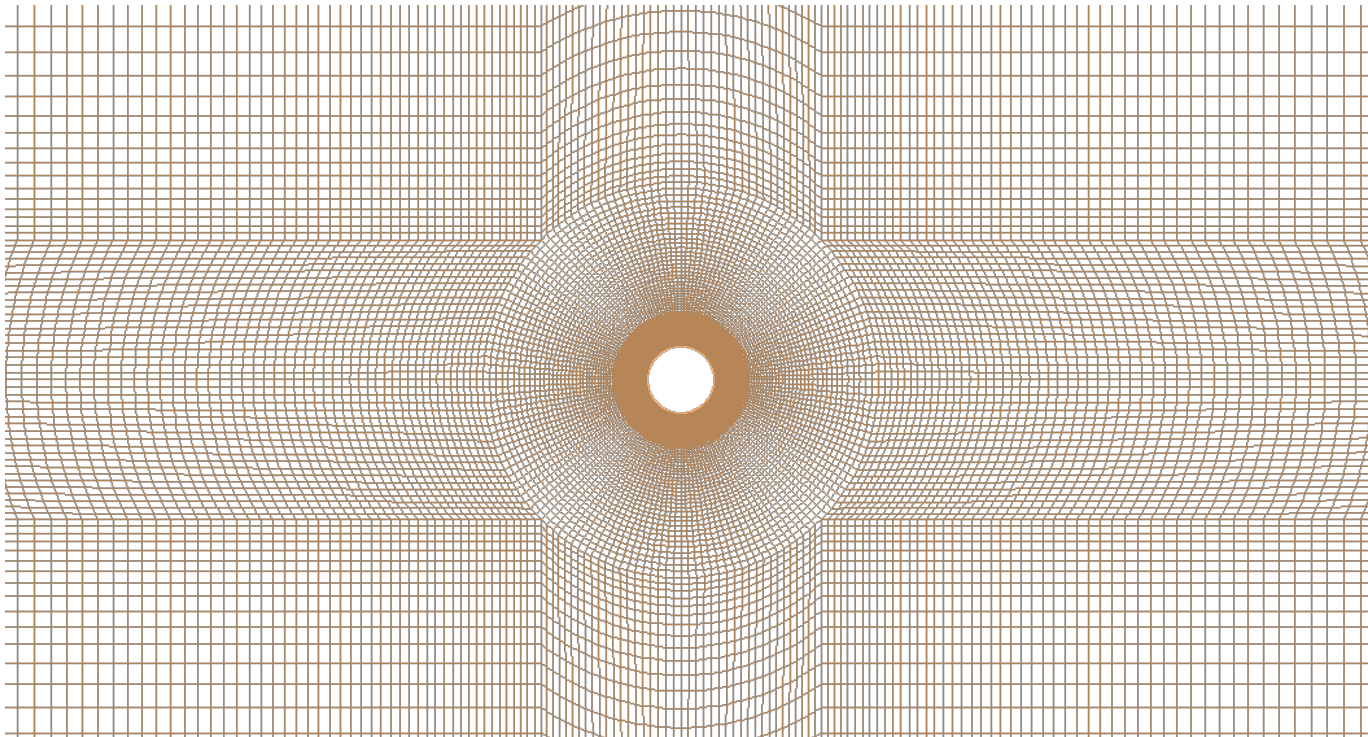
C_M is the inertia coefficient

C_D is the drag coefficient

- we also define:
$$C_x = \frac{F}{\frac{\rho}{2} U_m^2 D}$$

Grid in Fluent

Structured mesh is used in the calculation domain



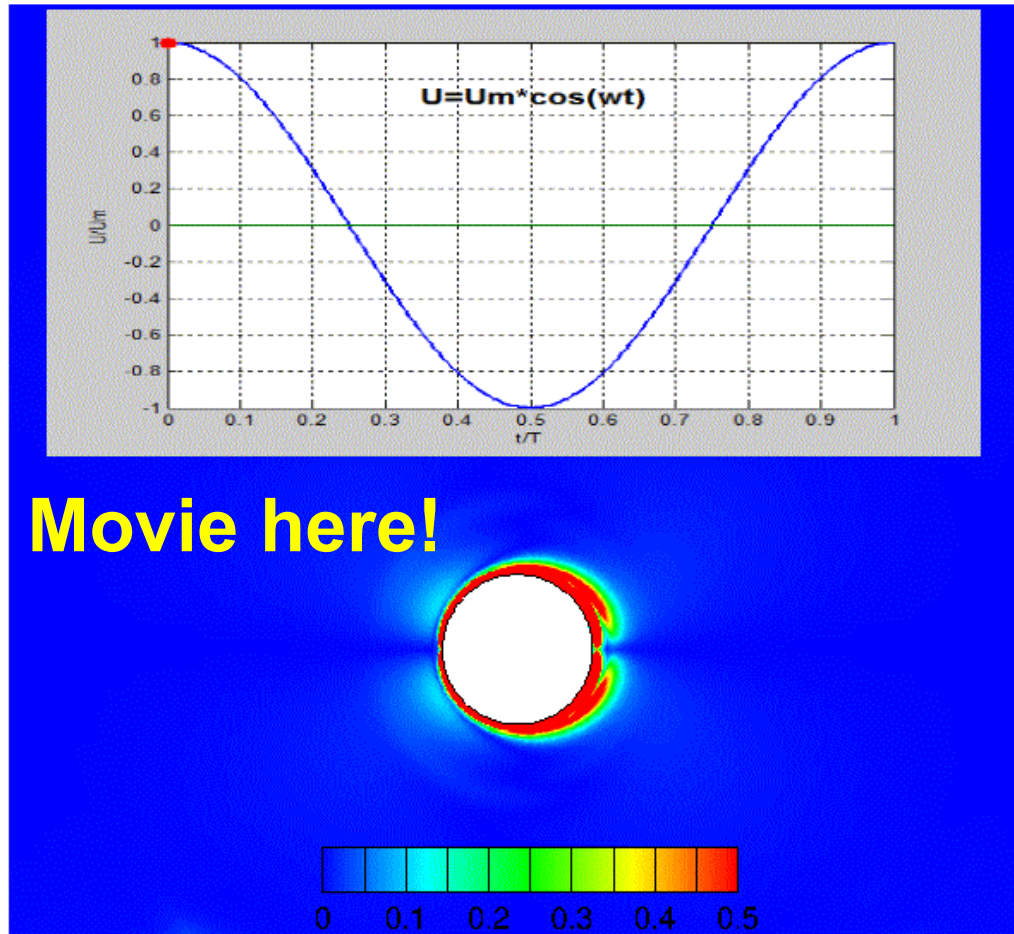
Mesh Info:

Cells: 76680

Faces: 154190

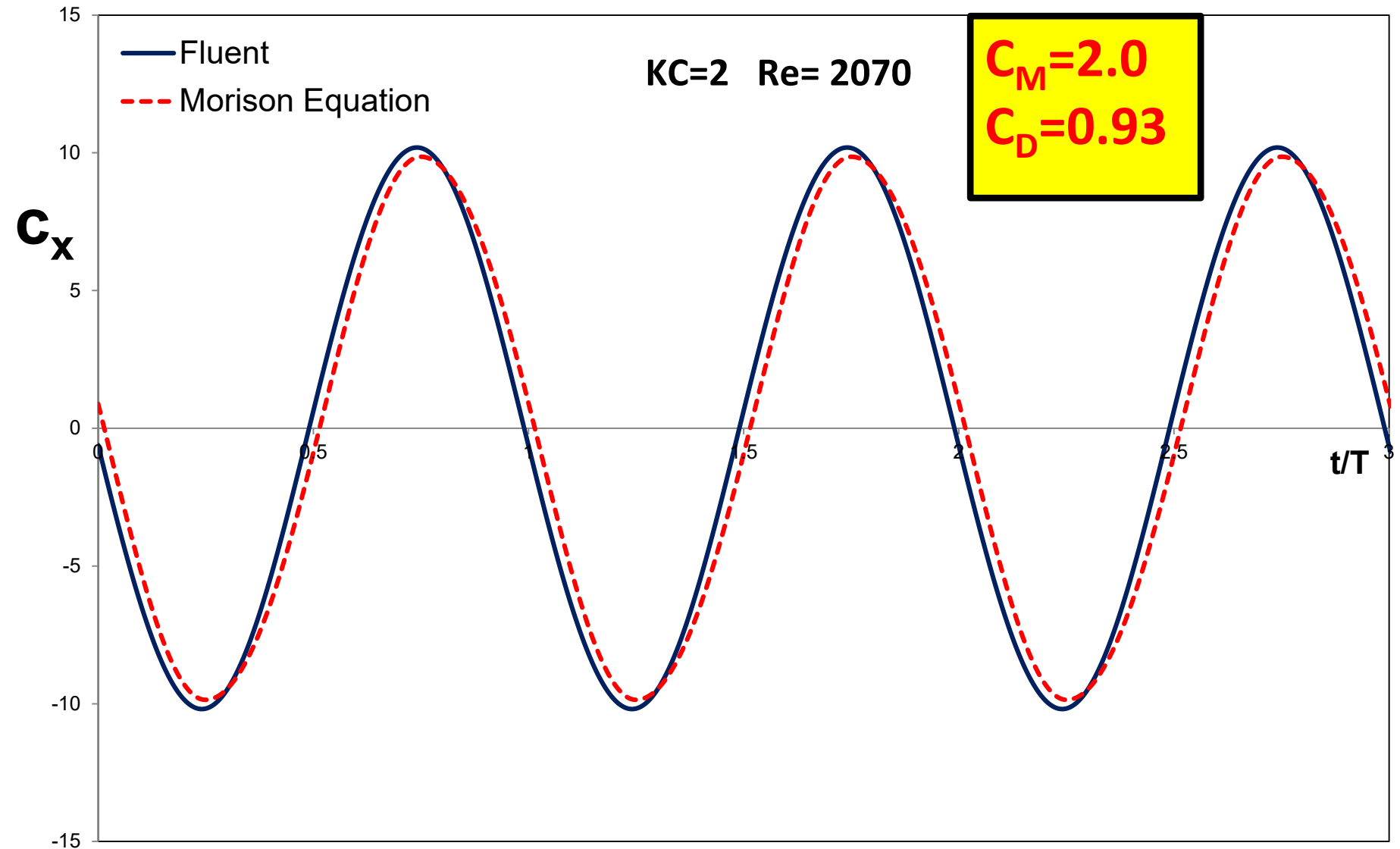
Nodes: 77510

Predicted flow (vorticity) by Fluent: $KC=2$, $Re=1070$
(click on the movie to play)

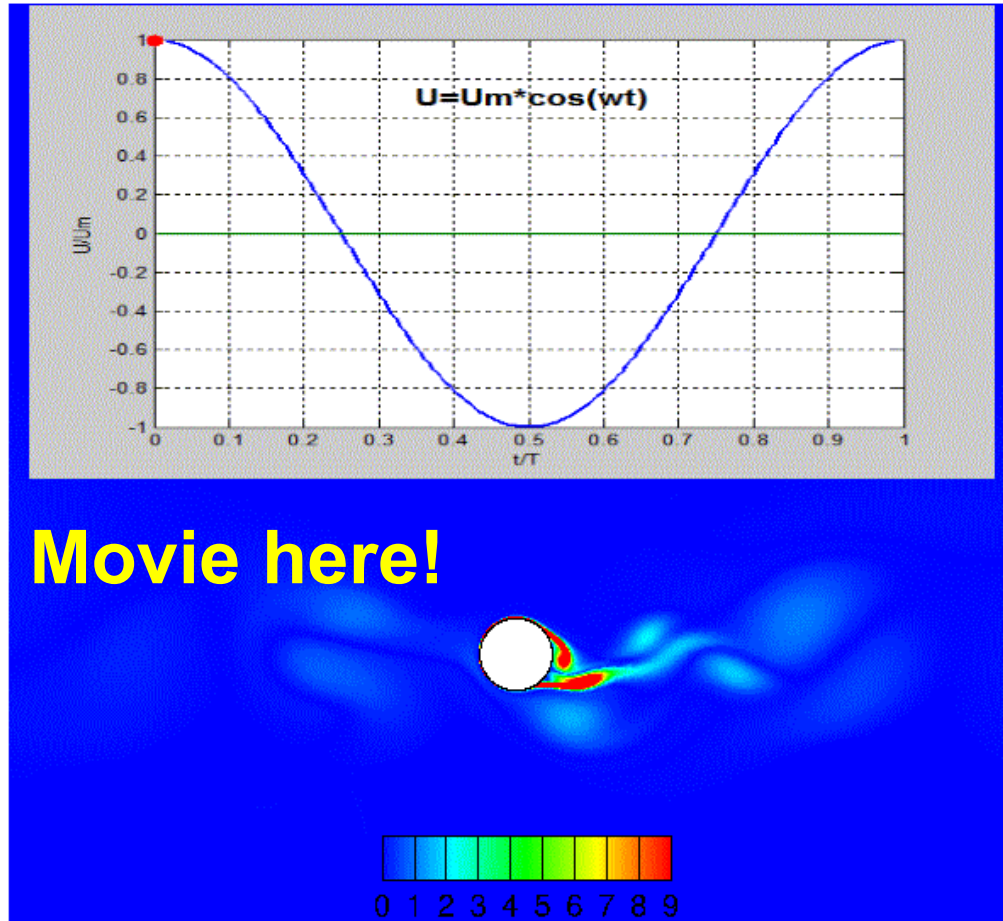


Movie here!

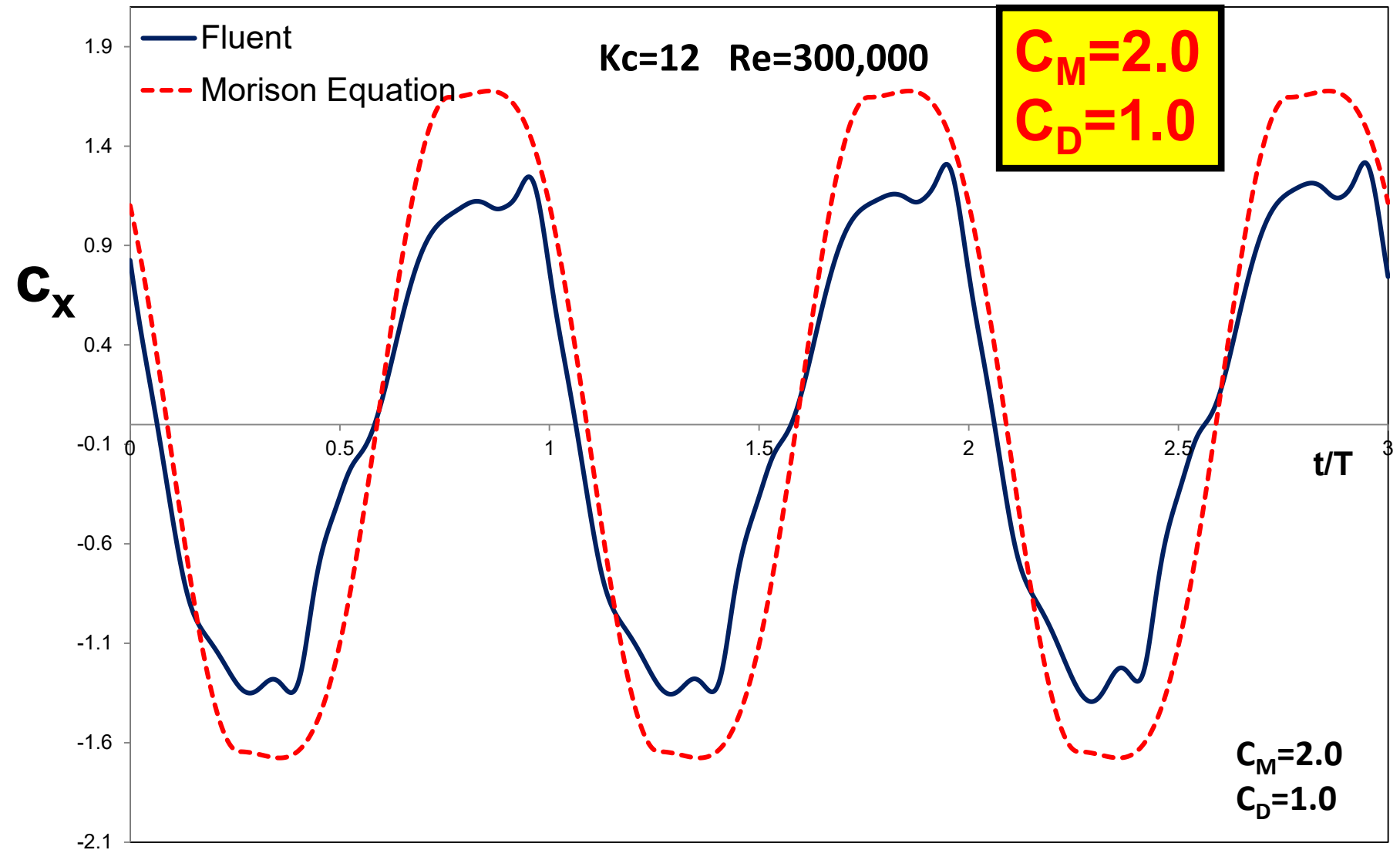
Case I: $KC=2$ $Re=1070$



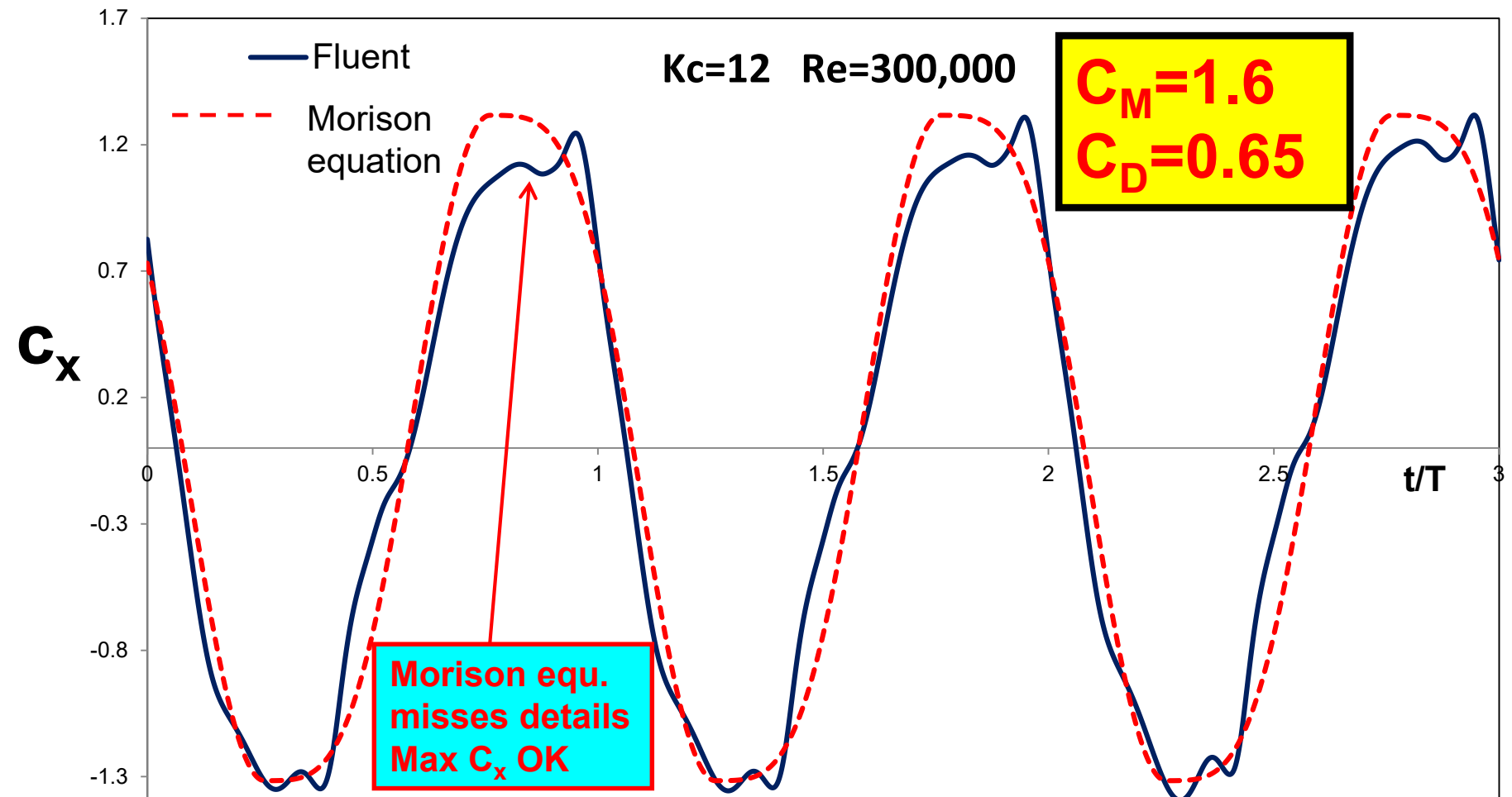
Predicted flow (vorticity) by Fluent: $KC=12$ $Re=300,000$
(click on the movie to play)



Case II: $KC=12$ $Re=300,000$



Case II: $KC=12$ $Re=300,000$



Maybe due to luck...more needs to be done!!! Some newer simulations will be shown in the lecture on Computational Hydrodynamics